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September 9, 2014



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Ms. Nancy Kempel Supervising Environmental Engineer Bureau of Surface Water Quality Division of Water Quality

Trenton, NJ 08625-0402

P.O. Box 402

RE: NJPDES Discharge Permit NJ 0226271
Plumsted Township Wastewater treatment Plant

Dear Ms. Kempel:

As discussed at our July 22, 2014 meeting, we are submitting this Addendum to the Socio Economic Analysis for the Plumsted Township Wastewater Treatment Plant (NJPDES Discharge Permit NJ 0226271) dated May 30, 2014. This Addendum responds to comments we received at our July meeting and subsequent conversations, particularly in regard to providing supporting information related to additional wastewater treatment options, in addition to the Advanced Membrane Filtration process with Reverse Osmosis, which may be less costly to construct and operate and which are capable of achieving the non degradation limits specified in the Department's letter dated January 13, 2014. At our July meeting it was agreed the Analysis did provide sufficient justification for the lowering of the non degradation water quality limit for Total Dissolved Solids (TDS). As also noted at the July meeting, we accept the non-degradation limits for CBOD₅, Total Suspended Solids, Dissolved Oxygen, Phosphorous and pH.

As suggested at our July 2014 meeting, we contacted Harrison Township to obtain information on their wastewater treatment system (STP). In Harrison Township, an Oxi-Ditch wastewater treatment process is used. We also include in this Addendum a modified Bardenpho wastewater treatment system which is in use at the Joint Base McGuire-Dix-Lakehurst (Joint Base). We did not consider any treatment system that could not achieve the reductions in phosphorous, ammonium and nitrate that are required. For both the above treatment processes, construction and operating costs were developed by Van Cleef Engineering for the initial 0.3 mgd discharge and the ultimate 0.6 mgd discharge and are included as attachments to this Addendum. A brief description of each treatment process is provided below (please refer to our May 30, 2014 submission for a description of the Advanced Membrane Filtration process):

Bardenpho System:

The Bardenpho wastewater treatment process is a rather complex system that utilizes biological means (with chemical additions) to achieve low N and P effluent values. It typically includes a four stage (as opposed to two stage) activated sludge treatment process. Due to the number of tanks involved in this treatment process, it is not only land intensive but the capital costs are greatly increased. The process is not designed to remove metals.

Oxidation Ditch System:

The Oxi-Ditch wastewater treatment process is a variation of the activated sludge process and typically operates in an extended aeration mode with long solids retention times. The process can be designed to achieve specific objectives including nitrification, denitrification and/or biological phosphorous removal. As with the Bardenphol system, the process is also not designed to remove metals and is land intensive.

To remove metals to the non-degradation limits specified, a separate metals removal process will be required. This will increase the construction costs of any treatment process that ultimately is selected. The Redevelopment Project is the financing mechanism for the proposed wastewater infrastructure (see May 30, 2014 Analysis). This increase in cost is not likely to be financeable as part of the planned Redevelopment project for New Egypt and this cost would have to be added to the annual user fees to operate and maintain the planned wastewater infrastructure including the wastewater treatment facility.

In summary, the estimated annual user costs without including any increase in construction costs for the antidegradation scenario for the Bardenpho and Oxi-Ditch wastewater treatment systems, as were the average annual user costs for the MBR/ Reverse Osmosis wastewater treatment system, are significantly higher than they are for the "Best Achievable" option (see Tables 1 and 2 attached). The average annual user fee, based on Jackson Township, Pemberton Township, Wrightstown Borough and the Jensen's Deep Run development in Plumsted Township) is \$450.00. For the Oxi-Ditch wastewater treatment process, the average annual user costs increase from \$601 per user (Best Available Technology) to \$1,219 per user for the 0.3 mgd discharge. For the Bardenpho Modified wastewater treatment process, the average annual user fee increases from \$601 per user (Best Achievable) to \$1,246 per user for the 0.3 mgd discharge. The construction costs for the Oxi-Ditch wastewater treatment plant increase from approximately \$4,112,000 (Best Achievable) to \$5,875,000 for the 0.3 mgd discharge. The construction costs for the Bardenpho Modified wastewater treatment plant increase from approximately \$4,112,000 to \$6,187,500 (see Tables 3 and 4 attached). As provided by the Department, we have completed and enclose the Tables that your office provided to us on August 14, 2014 (see Tables 5 and 6).

Given the above, we feel the lowering of the water quality limits for TDS as agreed to by the Department at our meeting of July 22, 2014 and the lowering of the water quality limits for Ammonia, Nitrate, Copper, Lead, Nickel and Zinc to be a reasonable and justified request and consistent with the anti-degradation policy contained in the Surface Water Quality Standards at N.J.A.C. 7:1.9.

We are hopeful this Addendum to our Socio-Economic Analysis will complete our submission and the Department will proceed to issue a draft permit for the proposed surface water discharge to the Crosswicks Creek. We are available to meet with you at any time that is convenient if you should have any additional comments.

Peter Ylvisaker

Cc: PMUA

Municipal Clerk

Chris Jepson, Van Cleef

Tables 1 and 2

Non- Degradation Annual Operations Cost Summary

Table 1: Non-Degradation Annual Operations Cost Summary 0.3 mgd Discharge

Treatment System	Annual Operating Cost	Annual User Cost*
MBR w/ Reverse Osmosis	\$1,106,594	\$1,006
Oxi-Ditch	\$1,340,983	\$1,219
Bardenpho Modified	\$1,370,433	\$1,246
_ MBR (Best Achievable)	\$ 671,594	\$ 611

^{*} Annual User Cost = Annual Operating Cost/1100

Notes: Average Annual User Fee = \$450

Table 2: Non-Degradation Annual Operations Cost Summary 0.6 mgd Discharge

Treatment System	Annual Operating Cost	Annual User Cost*
MBR w/ Reverse Osmosis	\$1,770,425	\$ 805
Oxi-Ditch	\$2,147,608	\$ 976
Bardenpho Modified	\$2,277,583	\$1,035
MBR (Best Achievable)	\$ 921,424	\$ 419

^{*} Annual User Cost = Annual Operating Cost/2200 Units

Notes: Average Annual User Fee = \$450

Tables 3 and 4

Non- Degradation Treatment System Construction Cost

Table 3: Non-Degradation Treatment System Construction Cost 0.3 mgd Discharge

Treatment System	Construction Cost	Increase Cost*
MBR w/ Reverse Osmosis	\$4,706,250	\$ 593.750
Oxi-Ditch	\$5,875,000	\$ 1,762,500
Bardenpho Modified	\$6,187,500	\$ 2,075,000
MBR (Best Achievable)	\$ 4,112,500	\$ 0

^{*} Increase = to Construction Cost - \$4,112,500 (Best Achievable)

Table 4: Non-Degradation Treatment System Construction Cost 0.6 mgd Discharge

Treatment System	Construction Cost	Increase Cost*
MBR w/ Reverse Osmosis	\$6,925,000	\$ 1,062,500
Oxi-Ditch	\$9,725,000	\$ 3,862,500
Bardenpho Modified	\$9,518,750	\$ 3,656,250
MBR (Best Achievable)	\$ 5,862,500	\$ 0

^{*} Increase = to Construction Cost - \$5,862,500 (Best Achievable)

Plumsted MUA WWTP		5 cfs, 7Q10 = 6 cfs , 30Q10 =	: 8 cfs, amblent u	=5 cfs, 7Q10 = 6 cfs , 30Q10 = 8 cfs, ambient upstream hardness = 59.9 mg/L, plant flow = 0.3 mgd	1c, plant flow = 0	S mgd		1010
Parameter	Non-Degradation Limits - Average Monthly Limit		Effluent limits an	Effluent limits and costs associated with various wastewater traatment processes	us wastewater t	reatment processes		Water Quality Based Ffloors Limits: Average Monthly Limits:
	(Na socio-economic analysis required)	MBR/chemical addition *	Cost per user \$	OxIDIz:h/chemical add	Cost per user \$	Bardenpho/chemical add	Cost per usar \$.	(Maximum)
			,	ПВ/L				
CBODs	1.0	1.0	\$611	2	81,219	1.5	\$1,246	971
Total Suspended Solids	6.01	6.01	\$611	8	\$1,219	7	\$1,246	e de la companya de l
Dissolved Oxygen	8.0 (Minimum)	8.0	\$611	8.0	£1,219	8.0	\$1,246	Solvanimum)
Phosphorus	0.1	0.1	\$611	0.3	\$1,219	0.1	\$1,246	
pH (standard units)	4.5 Minimum / 7.5 Maximum	4.5 Min/7.5 Max	\$611	4.5 Min/7.5 Max	\$17,13	4.5 Mln/7.5 Mex	\$1,246	45 Millimum (75 Westmum)
Total Dissolved Solids	163	1900	\$611	3100	\$1,219	2600	\$1,246	4856
Nitrate	0.35	מו	\$611	7	\$1,219	ທ	\$1,246	
Ammanla, Total as N	0.25	1	\$611	2	\$1,219	1	\$1,246	16982
				J/Brl				
Copper, Total Recoverable	2.54	25	\$611	95	\$1,219	7.5	\$1,246	69
Lead, Total Recoverable	1.52	20	\$611	85	\$1,219	59	\$1,246	
Vickel, Total Recoverable	0.85	22	\$611	100	\$1,719	06	\$1,246	4X6431
Zinc, Yotal Recoverable	21.5	35	\$611	100	\$1,219	06	\$1,246	30.0

Plumstad MUA to provide treatment processes evaluated and costs associated with those processes.
 (Examples of Treatment Processes: Biological Treatment, Blokgical/Chemical Treatment, Biological/Chemical Treatment with Filtration...)

[&]quot;These efficient limits were calculated assuming the following: assuming an efficient hardness of 100 mg/L

assuming the embient metals data was presented as from the report as dissolved using the sample frequency specified for this gbs discharger in NJA.C. 7:14A-14

All processes have chemical addition and tertiary fibration also for Oxi-Ditch and Bardenpho. MBR no tertiary filtration.

		1Q10 = 5 cfs, 7Q10 = 6 cfs ,	Plu 30Q10 = 8 cfs, an	Plumsted MUA WWTP 1Q10 = 5 cfs, 7Q10 = 6 cfs , 30Q10 = 8 cfs, embient upstream hardness = 59.9 mg/l, plant flow = 0.6 mgd	59.9 mg/L, plant	fow = 0.6 mgd		
Parameter	Non-Degradation Limits - Average Monthly Limit		Effluent limits an	Effluent limits and costs associated with various wastewater treatment processes	ous wastewater t	reatment processes		Water Cui IV Based Efficant Umita Autorit Child Chiliky Chilik
	(No socio-economic analysis required)	MBR/chemical addition	Cost per user \$	OxIDitch/chemical add	Cost per user \$	Bardenpho/chemical add	Cost per user \$	A SA HALL
				mg/L				ne state constituent of the cons
CBODs	1,0	1.0	\$419	2	\$978	15	\$1,035	
Total Suspended Solids	10.9	6.01	\$419	80	\$578	7	\$1,095	
Dissolved Oxygen	8.0 (Minimum)	8'0	\$419	8.0	\$578	8,0	\$1,035	
Phosphorus	0.1	0.1	\$419	0.3	\$2978	0.2 ·	\$1,035	
pH (stendard units)	4.5 Minimum / 7.5 Maximum	4.5 Min/7.5 Max	\$419	4.5 Min/7.5 Max	\$978	4.5 Min/7.5 Max	\$1,035	Authoriting // Eminimum
Total Dissolved Solids	163	1900	\$419	3100	\$97B	2600	\$1,035	26784
Nitrate	0.35	ın	\$419	7	\$978	lo.	\$1,035	
Ammonia, Total as N	0.25	1	\$419	2	\$978	1	\$1,035	124.0
				hg/L				
Copper, Total Recoverable	2.54	25	\$419	85	\$978	75	\$1,035	422
Lead, Total Recoverable	1.52	16	\$419	85	\$7.6\$	65	\$1,035	GÜ
Nickel, Total Recoverable	0.85	25	\$419	100	\$978	06	\$1,035	Livia Livia
Zinc, Total Recoverable	21.5	35	\$419	100	\$978	06	\$1,035	9014

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^{*} Plumsted MUA to provide treatment processes evaluated and costs associated with those processes. [Examples of Treatment Processes: Biological Treatment, Biological/Chemical Treatment, Biological/Chemical Treatment with Filtration...)

^{**} These effluent limits were calculated assuming the following:

assuming an effluent hardness of 100 mg/L assuming the ambient metals data was presented as from the report as dissolved using the sample frequency specified for this size discharger in N.J.A.C. 7.14A-14

Attachment 1

Operating and Construction Cost Estimates



MBR Wastewater Treatment Facility (300,000 GPD)

Generator Fuel	
Pumping station generator fuel costs.=	975
1 hr/wk exercise x 52 wks x 4 gal/hr x \$4/gal.=	\$832
3/4 Load - 24 hrs/yr x 7 gal/hr x \$4/gal.=	\$672
Total Cost per Year =	\$2,479
Operator Costs	
20 hrs/week x 52 weeks/yr x \$80/hr =	\$83,200
Total Cost per Year =	\$83,200
Laboratory Costs	
	•
Monthly influent & effluent samples to outside lab. =	\$1,900
Monthly influent & effluent samples - onsite testing =	\$500
Annual sludge testing =	\$200
Annual effluent volatile organics & heavy metals =	\$1,000
Total Cost per Year =	\$3,600
Chemical Costs	
Alum for phosphorus removal - 77 lbs/day x 365 days x \$0.3/lb =	ED 400
MBR cleaning (sodium hypochlorite)	\$8,432
Alkalinity adjustment - \$5/day x 365 days =	\$3,506
Total Cost per Year =	\$1,825 \$13,763
real cost por real -	\$15,705
Sludge Removal & Disposal	
(4% solids) 1554 gal/day x 365 days/yr x \$0.2/gal =	\$113,442
Total Cost per Year =	\$113,442
Electrical Costs	
MBR System	\$68,800
WWTP.	15,979
Pumping station	9,500
Washington -	•
Membrane Replacement Costs	
MBR	28,800
Odor Control	¥
and the second s	
Activated Carbon - 2,000 lb unit x 2/yr x \$2.5/lb =	\$10,000
Total Cost per Year =	\$10,000

Total Operation Costs = \$339,563 Per Year
Per Month



4/2/2014

MBR Wastewater Treatment Facility (300,000 GPD) with Supplemental Reverse Osmosis System

Generator Fuel	
Pumping station generator fuel costs.=	975
1 hr/wk exercise x 52 wks x 4 gal/hr x \$4/gal.=	\$832
3/4 Load - 24 hrs/yr x 7 gal/hr x \$4/gal.=	\$672
Total Cost per Year =	\$2,479
Operator Costs	
20 hrs/week x 52 weeks/yr x \$80/hr = _	\$83,200
Total Cost per Year =	\$83,200
,	
Laboratory Costs	
Monthly influent & effluent samples to outside lab. =	\$1,900
Monthly Influent & effluent samples - onsite testing =	\$500
Annual sludge testing =	\$200
Annual effluent volatile organics & heavy metals = _	\$1,000
Total Cost per Year =	\$3,600
·	
Chemical Costs	
Alum for phosphorus removal - 77 lbs/day x 365 days x \$0.3/lb =	\$8,432
RO chemical cleaner (acid and caustic)	\$579
RO anti-scalant	\$2,201
MBR cleaning (sodium hypochlorite)	\$3,506
Alkalinity adjustment - \$5/day x 365 days = _	\$1,825
Total Cost per Year =	\$16,543
Sludge Removal & Disposal	
(4% solids) 1554 gal/day x 365 days/yr x \$0.2/gal = _	\$113, 44 2
Total Cost per Year =	\$113,442
Electrical Costs	
MBR System	\$68,800
WWTP	15,979
Reverse Osmosis System	24,339
Pumping station	9,500
,	
Membrane Replacement Costs	
MBR, RO, RO concentrator	53,900
RO Reject Water Disposal (100% flow treated)	222 200
6000 GPD x 365 x \$0.17/gal	372,300
Odor Control	\$10,000
Activated Carbon - 2,000 lb unit x 2/yr x \$2.5/lb =	\$10,000
Total Cost per Year ≃	יטטטייטו פּ

\$774,082 Per Year Total Operation Costs = Per Month



4/2/2014

MBR Wastewater Treatment Facility (600,000 GPD)

Generator Fuel			
	Pumping station generator fuel costs.=	97	75
1 hr	/wk exercise x 52 wks x 4 gal/hr x \$4/gal =	600	in the second se
•	Full Load - 24 hrs/yr x 10 gal/hr x \$4/gal.=	\$89	
	Total Cost per Year =	\$2,70	
Operator Costs		42,70	
	20 hrs/week x 52 weeks/yr x \$80/hr =	\$83,20	ń
	Total Cost per Year =	\$83,20	
l abornéen. Casé		,,	-
Laboratory Costs			
Monthly in	fluent & effluent samples to outside lab. =	\$1,900)
MOUTHIN ILI	uent & effluent samples - onsite testing =	\$500)
Annual	Annual sludge testing =	\$200	
Villing! 6	ffluent volatile organics & heavy metals =	\$1,000	
	Total Cost per Year =	\$3,600	
Chemical Costs			
	oval - 154 lbs/day x 365 days x \$0.3/lb =		
MBR cle	aning (sodium hypochlorite)	\$16,864	
Alka	alinity adjustment - \$10/day x 365 days =	\$3,506	
	Total Cost and W	\$3,650	
	Total Cost per Year =	\$24,020	
Sludge Removal &	Disposal		
(4% solids)	3108 gal/day x 365 days/yr x \$0.2/gal =	F000 004	
2	Total Cost per Year =	\$226,884	
	Total Cost per real c	\$226,884	
Electrical Costs			
MBR Syst	em	\$137,600	
WWTP		21,305	
Pumping 8	Station	12,000	
Manual		12,000	
Membrane Replacen	ent Costs		
MBR		57,600	
Odor Control		,	
	N. C		~
Activated (Carbon - 2,000 lb unit x 4/yr x \$2.5/lb =	\$20,000	
	Total Cost per Year =	\$20,000	
	Total Operation	Costs =	\$588,912 Per Year
*/			Per Month



MBR Wastewater Treatment Facility (600,000 GPD)

With Supplemental Reverse Osmosis System

Generator Fuel	
Pumping station generator fuel costs.=	975
1 hr/wk exercise x 52 wks x 4 gal/hr x \$4/gal.=	\$832
Full Load - 24 hrs/yr x 10 gal/hr x \$4/gal.=	\$896
Total Cost per Year =	
Operator Costs	Ţ.,,
20 hrs/week x 52 weeks/yr x \$80/hr =	\$83,200
Total Cost per Year =	\$83,200
,	, ,
Laboratory Costs	
Monthly influent & effluent samples to outside lab. =	\$1,900
Monthly influent & effluent samples - onsite testing =	\$500
Annual sludge testing =	\$200
Annual effluent volatile organics & heavy metals =	\$1,000
Total Cost per Year =	\$3,500
Chemical Costs	
Alum for phosphorus removal - 154 lbs/day x 365 days x \$0.3/lb =	\$16,864
RO chemical cleaner (acid and caustic)	\$1,157
RO anti-scalant	\$4,411
MBR cleaning (sodium hypochlorite)	\$3,506
Alkalinity adjustment - \$10/day x 365 days = _	\$3,650
Total Cost per Year =	\$29,588
Sludge Removal & Disposal	
(4% solids) 3109 gal/day x 365 days/yr x \$0.2/gal =	P000 004
Total Cost per Year =	\$226,884
Total cost bet Teat =	\$226,884
Electrical Costs	
MBR System	\$137,600
WWTP	21,305
Reverse Osmosis System	48,678
Pumping Station	12,000
•	12,000
Membrane Replacement Costs	
MBR, RO, RO concentrator	107,800
	,
RO Reject Water Disposal (100% flow treated)	
12000 GPD x 365 x \$0.17/gal	744,600
	and proper contracting to
Odor Control	
Activated Carbon - 2,000 lb unit x 4/yr x \$2.5/lb =	\$20,000
Total Cost per Year =	\$20,000

Total Operation Costs = \$1,437,913 Per Year

Per Month



Plumsted Township MUA Construction Cost Summary for Phase 1 & 2 MBR Wastewater Treatment Systems

	Dynatec MBR 300,000 GPD	Dynatec MBR 600,000 GPD	
Building	\$235,000	\$235,000	
Concrete Bldg. Floor & foundation	\$40,000	\$40,000	
Concrete for Steel Tank Foundations	\$65,000	\$65,000	
Concrete Tankage	-	-	
Electrical & Genset	\$300,000	\$300,000	
Interconnecting Pipe & Pipe Insulation	\$80,000	\$80,000	
Tanks & equipment	\$1,800,000	\$3,100,000	
Construction Installation	\$500,000	\$600,000	
Flow Equalization Tanks	\$270,000	\$270,000	
25% contingency_	\$822,500 \$4,112,500	\$1,172,500 \$5,862,500	

1. Steel fabricated tanks - membrane filtration

All include chemical feed systems for phosphorus removal



Plumsted Township MUA Cost Summary for Phase 1 & 2 MBR Wastewater Treatment Systems with Supplemental Reverse Osmosis

	Dynatec MBR 300,000 GPD	Dynatec MBR 600,000 GPD	
Building		\$235,000	
Concrete Bldg, Floor & foundation	\$40,000	\$40,000	
Concrete for Steel Tank Foundations	\$65,000	\$65,000	
Concrete Tankage	-		
Electrical & Genset	\$300,000	\$300,000	
Interconnecting Pipe & Pipe Insulation	\$80,000	\$80,000	
Tanks & equipment	\$1,800,000	\$3,100,000	
Construction Installation	\$500,000	\$600,000	
Reverse Osmosis System	\$375,000	\$700,000	
Construction Installation	\$100,000	\$150,000	
Flow Equalization Tanks	\$270,000	\$270,000	
25% contingency	\$941,250 \$4,706,250	\$1,385,000 \$6,925,000	

^{1.} Steel fabricated tanks - membrane filiration

All include chemical feed systems for phosphorus removal



Oxi-ditch Wastewater Treatment Facility (300,000 GPD)

Generator Fuel		
1 hr/wk exe	rcise x 52 wks x 7 gal/hr x \$4/gal.=	\$1,45
Full Los	ad - 24 hrs/yr x 15 gal/hr x \$4/gal.=	\$1,44
	Total Cost per Year =	\$2,890
Operator Costs		•
. 25	hrs/week x 52 weeks/yr x \$80/hr =	\$104,000
	Total Cost per Year =	\$104,000
Laboratory Costs		
	effluent samples to outside lab. =	
Monthly influent &	effluent samples - onsite testing =	\$1,900
, masin a	Annual sludge testing =	\$750
Annual effluent v	olatile organics & heavy metals =	\$800
	Total Cost per Year =	\$1,000
	rotar cost per rear =	\$4,450
Chemical Costs		
Alum for phosphorus removal - 20	00 lbs/day x 365 days x \$0 3/lb =	\$21,900
	Acid (metals removal)	\$2,000
	Base (metals removal)	\$2,000
Neutralizer (meta	als removal)	\$2,500
Alkalinity ad	justment - \$45/day x 365 days =	\$16,425
	Total Cost per Year =	\$44,825
Sludge Rameral & D.		,
Sludge Removal & Disposa	d 16 1	
(4% solids) 3150 ga	l/day x 365 days/yr x \$0.2/gal =	\$229,950
	Total Cost per Year =	\$229,950
Electrical Costs		
Oxidation Ditch Sy	/stem	
WWTP (blowers,	ato)	\$41,000
Pumping Stations	3.0.7	140,000
		38,000
Effluent Disk Replacement (Cost	40.000
		12,000
Metals Sludge Disposal		
3000 GPD x 365 x	\$0.33/gal	361,350
Odor Control		-51,000
	0.000 !!	
Activated Carbon -	2,000 lb unit x 6/yr x \$2.5/lb =	\$30,000
	Total Cost per Year =	\$30,000

Total Operation Costs = \$1,008,471 Per Year

Per Month



Oxi-ditch Wastewater Treatment Facility (600,000 GPD)

Generator Fuel		
1 hr/w	k exercise x 52 wks x 7 gal/hr x \$4/gal.=	\$1,456
F	ull Load - 24 hrs/yr x 15 gal/hr x \$4/gal.=	\$1,440
	Total Cost per Year =	\$2,896
Operator Costs		
	30 hrs/week x 52 weeks/yr x \$80/hr =	\$124,800
	Total Cost per Year =	\$124,800
Laboratory Costs		
	uent & effluent samples to outside lab. =	
Monthly Influ	ent & effluent samples - onsite testing =	\$1,900
wienany milat		\$750
Annual eff	Annual sludge testing = uent volatila organics & heavy metals =	\$800
, and a diff	Total Cost per Year =	\$1,000
	Total cost per fear =	\$4,450
Chemical Costs		
Alum for phosphorus remov	val - 350 lbs/day x 365 days x \$0.3/lb =	\$38,325
	Acid (metals removal)	\$4,000
	Base (metals removal)	\$4,000
Neutralize	r (metals removal)	\$5,000
Alkalii	nity adjustment - \$85/day x 365 days =	\$31,025
	Total Cost per Year =	\$82,350
DI	-	•
Sludge Removal & Di	isposai	
(4% SOIIDS) 6	300 gal/day x 365 days/уг x \$0.2/gal = _	\$459,900
	Total Cost per Year =	\$459,900
Electrical Costs		
	Ditch System	
WWTP (blo	NAGE ato	\$82,000
Pumping St		224,000
, amping of	20013	48,000
Effluent Disk Replace	ment Cost	24,000
	- Section 19 (1990)	24,000
Metals Sludge Dispos		
6000 GPD x	365 x \$0.33/gal	722,700
Odor Control		
Activated Ca	arbon - 2,000 lb unit x 8/yr x \$2.5/lb =	\$40,000
	Total Cost per Year =	\$40,000

Total Operation Costs = \$1,815,096 Per Year
Per Month

8-15-14



Plumsted Township MUA Construction Cost Summary for Phase 1 & 2 Oxldation Ditch Wastewater Treatment Systems

	OVIVO	OVIVO	
	O2 Ditch	O2 Ditch	
D. II II	300,000 GPD	600,000 GPD	
Building	9 \$235,000	\$235,000	
Concrete Bldg, Floor & foundation	\$40,000	\$40,000	
Influent Coarse Screen (Hydrodyne)	\$115,000	\$145,000	
Grit Removal (Pista Grit)	\$45,000	\$55,000	
Fine screen	\$40,000	\$75,000	
Electrical & Genset	\$450,000	\$450,000	
Interconnecting Pipe & Pipe Insulation	\$145,000	\$205,000	
Blowers (Pista Grit, Sludge Tank, re-air)	\$55,000	\$85,000	
Primary Clarifiers (chains, flights, weirs)	\$125,000	\$240,000	
Ovivo Oxidation Ditch & equipment	\$1,400,000	\$2,700,000	
Secondary Clarifiers (chains, flights, weirs)	\$125,000	\$240,000	
P removal Clarifler (mixer, weirs)	\$95,000	\$180,000	
Metals removal Unit (pH,mixers,weirs)	\$85,000	\$160,000	
Disk Filter (Kruger) & equipment	\$650,000	\$1,200,000	
UV disinfection	\$50,000	\$90,000	
Re-aeration tank (coarse bubble diffusion)	\$45,000	\$80,000	
Construction Installation \$	1,000,000	\$1,600,000	*
25% contingency \$		\$1,945,000	
. 3	5,875,000	\$9,725,000	

All include chemical feed systems for phosphorus/metals removal



Bardenpho Wastewater Treatment Facility (300,000 GPD)

Generator Fuel		
1 hr/wk	exercise x 52 wks x 8 gal/hr x \$4/gal.=	\$1,664
Ful	l Load - 24 hrs/yr x 17 gal/hr x \$4/gal.=	\$1,632
	Total Cost per Year =	\$3,296
Operator Costs		
	25 hrs/week x 52 weeks/yr x \$80/hr =	\$104,000
	Total Cost per Year =	\$104,000
Laboratory Costs		
	nt & effluent samples to outside lab. =	
Monthly influer	of & officent samples to outside lab. =	\$1,900
inchary initial	nt & effluent samples - onsite testing =	\$750
uffe leunnA	Annual sludge testing =	\$800
/ unidal Gilige	ent volatile organics & heavy metals =	\$1,000
	Total Cost per Year =	\$4,450
Chemical Costs		
	al - 100 lbs/day x 365 days x \$0.3/lb =	#40 DCD
1	Acid (metals removal)	\$10,950
		\$2,000
Neutralizer (Base (metals removal) metals removal)	\$2,000
Alkalini	ty adjustment - \$45/day x 365 days =	\$2,500
, dican	Total Cost and Yarra	\$16,425
,	Total Cost per Year =	\$33,875
Sludge Removal & Dis	posal	
(4% solids) 315	50 gal/day x 365 days/yr x \$0.2/gal =	£220 0E0
, , , , , , ,	Total Cost per Year =	\$229,950 \$229,950
	Total Goot per Tear =	\$229,950
Electrical Costs		
Bardenpho S	ystem	\$41,000
WWTP (blow	vers, etc.)	180,000
Pumping Stat	tions	38,000
		36,000
Effluent Disk Replacem	ent Cost	12,000
		12,002
Metals Sludge Disposal		
3000 GPD x 3	365 x \$0.33/gal	361,350
04 0 (-)		
Odor Control		
Activated Cart	oon - 2,000 lb unit x 6/yr x \$2.5/lb =	\$30,000
	Total Cost per Year =	\$30,000

Total Operation Costs = \$1,037,921 Per Year

Per Month



Bardenpho Wastewater Treatment Facility (600,000 GPD)

Generator Fuel		
1 hr/wk exercise x	52 wks x 8 gal/hr x \$4/gal.=	\$1,664
Full Load - 24	hrs/yr x 17 gal/hr x \$4/gal.=	\$1,632
	Total Cost per Year =	\$3,296
Operator Costs	* 90.00	
30 hrs/wee	ek x 52 weeks/yr x \$80/hr =	
	Total Cost per Year =	\$124,800
Laboratory Costs		
	nt samples to outside lab. =	
Monthly influent & effluent	samples to outside lab. =	\$1,900
monany mindent & enident	samples - onsite testing =	\$750
Annual officent valetie	Annual sludge testing =	\$800
Allidat etildent voiatile	organics & heavy metals =	\$1,000
	Total Cost per Year =	\$4,450
Chemical Costs		
Alum for phosphorus removal - 200 lbs/o	dov v 785 dov do 6.00	
Table Pricepholas Temoval - 200 Ibs/0	lay x 305 days x \$0.3/lb =	\$21,900
	Acid (metals removal)	\$4,000
Noutralian (Base (metals removal)	\$4,000
Neutralizer (metals rem	oval)	\$5,000
Arkalinity adjustme	nt - \$85/day x 365 days = _	\$31,025
	Total Cost per Year =	\$65,925
Sludge Removal & Disposal		
(4% solids) 6300 galldown	205	20.00
(4% solids) 6300 gal/day x	365 days/yr x \$0.2/gal =	\$459,900
	Total Cost per Year =	\$459,900
Electrical Costs		
Bardenpho System		***
WWTP (blowers, etc.)		\$82,000
Pumping Stations		360,000
r umping Stations		58,000
Effluent Disk Replacement Cost		0.1.000
		24,000
Metals Sludge Disposal		
6000 GPD x 365 x \$0.33/	oal	722 700
	5	722,700
Odor Control		
Activated Carbon - 2,000	lb unit x 8/vr x \$2.5/lb =	\$40,000
	Total Cost per Year =	\$40,000

Total Operation Costs = \$1,945,071 Per Year

Per Month



Plumsted Township MUA Construction Cost Summary for Phase 1 & 2 Modified Bardenpho Wastewater Treatment Systems

	Bardenpho Modified -300,000 GPD	Bardenpho Modified 600,000 GPD	
Buildin	\$305,000	\$305,000	
Concrete Bldg. Floor & foundation	\$60,000	\$60,000	
Influent Coarse Screen (Hydrodyne)	\$115,000	\$145,000	
Grit Removal (Plsta Grit)	\$45,000	\$55,000	
Fine screen	\$40,000	\$75,000	
Electrical & Genset	\$500,000	\$500,000	
Interconnecting Pipe & Pipe Insulation	\$205,000	\$265,000	
Blowers(Aera, Grit, Sludge Tank,2 re-air)	\$100,000	\$150,000	
Primary Clarifiers (chains, flights, weirs)	\$125,000	\$240,000	
Bardenpho Process & equipment	\$1,600,000	\$2,600,000	
Secondary Clarifiers (chains,flights,weirs)	\$125,000	\$240,000	
No separate P removal tank	\$0	\$0 .	
Metals removal Unit (pH,mixers,weirs)	\$85,000	\$160,000	
Disk Filter (Kruger) & equipment	\$650,000	\$1,200,000	
UV disinfection	\$50,000	\$90,000	
Re-aeration tank (coarse bubble diffusion)	\$45,000	\$80,000	
Construction Installation	\$900,000	\$1,450,000	
25% contingency \$		\$1,903,750	
\$6	3,187,500	\$9,518,750	

All include chemical feed systems for phosphorus/metals removal